



DOE Bioenergy Technologies Office (BETO) 2023 Project Peer Review

Designing Recyclable Biomass-Based Polyesters

April 4, 2023

Plastic Deconstruction and Resdesign

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This presentation does not contain any proprietary, confidential, or otherwise restricted information

Quad Chart Overview

Timeline

- *Project start date: October 1, 2021*
- *Project end date: September 30, 2024*

	FY22 Costed	Total Award
DOE Funding	\$643,662	\$2,500,000
Project Cost Share *	\$201,904	\$625,000

Project Goal

The overall goal of this project is to design new biomass-based polyesters that have improved thermal or mechanical properties compared to polybutylene adipate terephthalate (PBAT) and also are chemically recyclable and biodegradable.

End of Project Milestone

Demonstrate the production of at least one biomass-based polyester having the environmental, economic targets. .

Funding Mechanism
DE-FOA-0002245

TRL at Project Start: 2
TRL at Project End: 4

Project Partners*

- University of Oklahoma
- National Renewable Energy Laboratory
- Colorado State
- StoraEnso, Amcor, Pyran

*Only fill out if applicable.

1. Approach: Objectives for BOTTLE Project

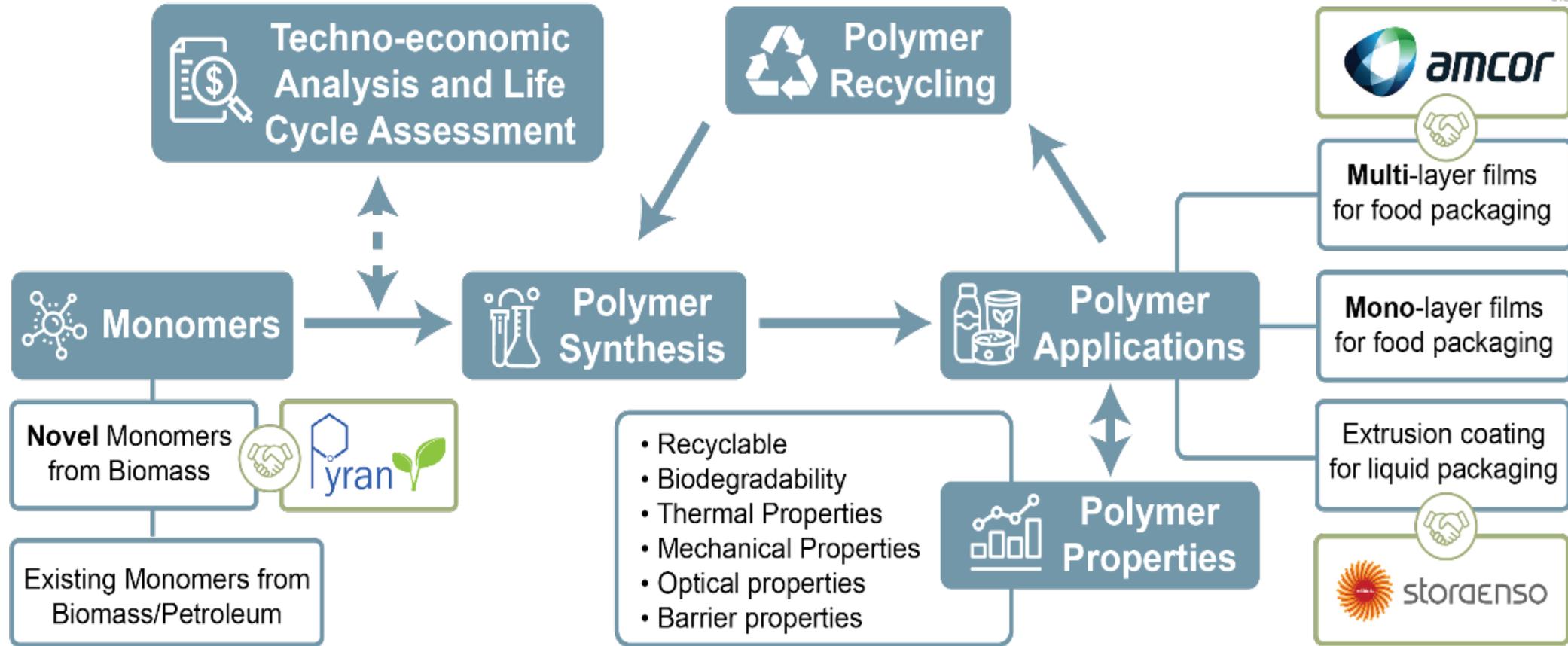
The overall goal of this project is to design **new biomass-based polyesters** that have improved thermal or mechanical properties compared to PBAT and are also chemically recyclable and biodegradable. We will test these polyesters in three different commercial applications.

The goal of this project is to design a new class of polyesters with the following properties:

1. **50 to 70%** lower energy input than conventional petroleum polymers.
2. Biomass based content from **50 to 100 wt%**.
3. Costs **30-50%** lower than PBAT.
4. **60%** biodegradable in 180 days by ASTM D6400.
5. Modulus at least **200 MPa** and elongation at break at least 350% (similar to LDPE and linear-low density poly-ethylene (LLDPE)).
6. Melting temperature **105-115°C** (similar to LDPE and LLDPE).
7. Haze index for a 25 μm film ~ 10 according to ASTM D1003 (similar to LDPE and LLDPE).
8. O₂ transmission rate equal to or lower than $\sim 8000 \text{ cm}^3/(\text{m}^2 \text{ day})$ (LDPE and LLDPE).₃

1. Approach:

Designing Recyclable Biomass-Based Polyesters



Department of Energy

U.S. Department of Energy Announces
\$27 Million in Plastics Recycling
Research and Development

OCTOBER 15, 2020

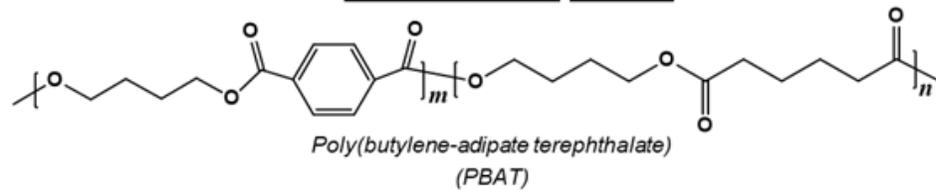


The UNIVERSITY
of OKLAHOMA

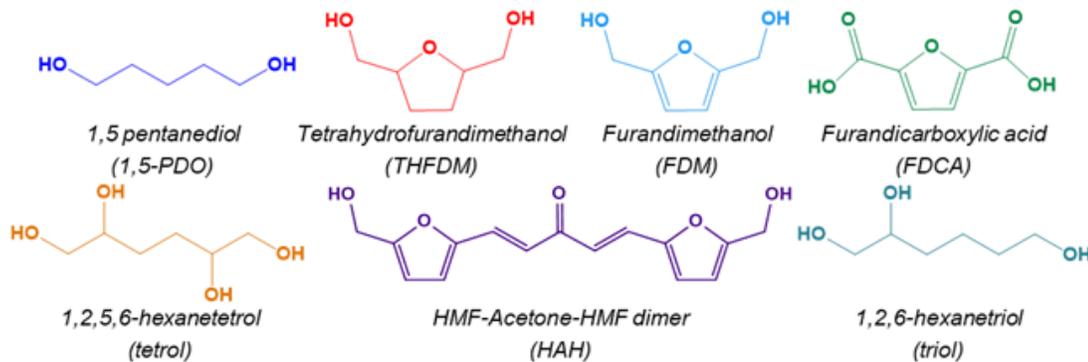


WISCONSIN
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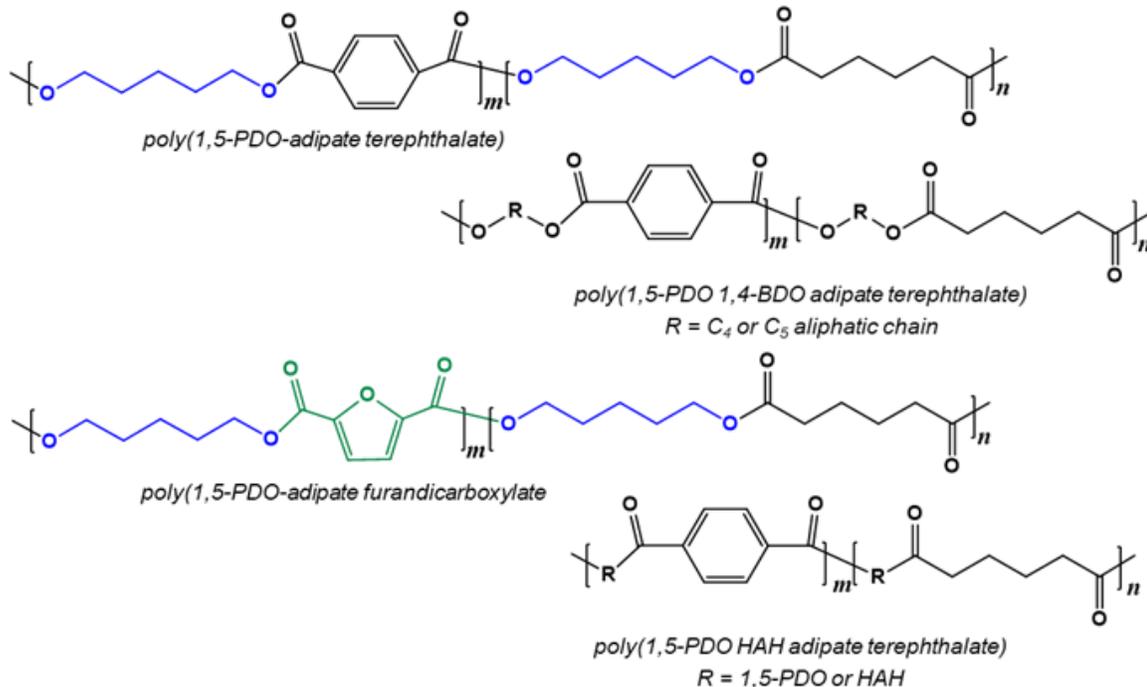
Petroleum-based Polymer



Biomass-based Monomers



Biomass-based Polymers



1. Approach

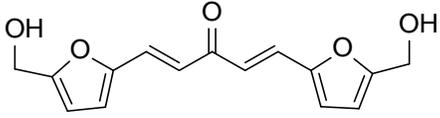
- PBAT is a biodegradable polymer (260 ktons/year) that is sold as a biodegradable polymer (blended with PLA) mainly for agricultural mulching applications.
- PBAT is blended with PLA to improve mechanical properties
- Challenge is that PBAT is expensive and has worse mechanical properties than LDPE requiring more PBAT for the same
- Team has 15+ years in making monomers from biomass.
- Pyran is commercializing the route to produce 15 PDO from biomass.
- StoraEnso is commercializing the route to produce HMF and FDCA from biomass.
- UW has a patent to produce tetrol application (up to 50% amount of PBAT)
- Key hypothesis of this proposal is that we will be able to design new types of biodegradable polyaliphatic-polyaromatic polyesters that have improved properties compared to PBAT.

1. Approach: Technical Scope Summary for BOTTLE Project

The project is divided into three budget periods over a **3-year period**.

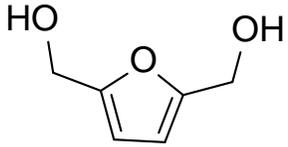
- Budget period 1 (3 months): Verify to the DOE verification team that the information we provided in the proposal is correct. (10/1/2021-1/1/2022)
- Budget period 2 (18 months): Synthesize one new biomass-based polyester that meets the proposed physical and economic targets outlined in this project. (1/1/2022- 8/31/2023)
- Budget period 3 (15 months): Test the biomass-based polyesters in three different commercial applications. (8/31/2023-12/1/2024)

2. Outcomes: Have been able to Synthesize and Purify a Wide Range of Monomers



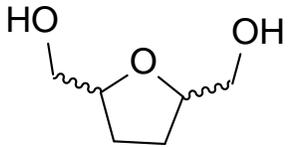
HMF-acetone-HMF dimer
(HAH)

→ 20 g per day in a 1L batch reactor



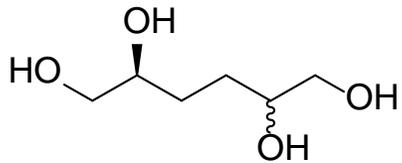
furandimethanol
(FDM)

→ 8 g per day in a 75 ml batch reactor OR 40 g per day in a continuous flow reactor



tetrahydrofuran-
dimethanol
(THFDM)

→ 8 g per day in a 75 ml batch reactor OR 40 g per day in a continuous flow reactor



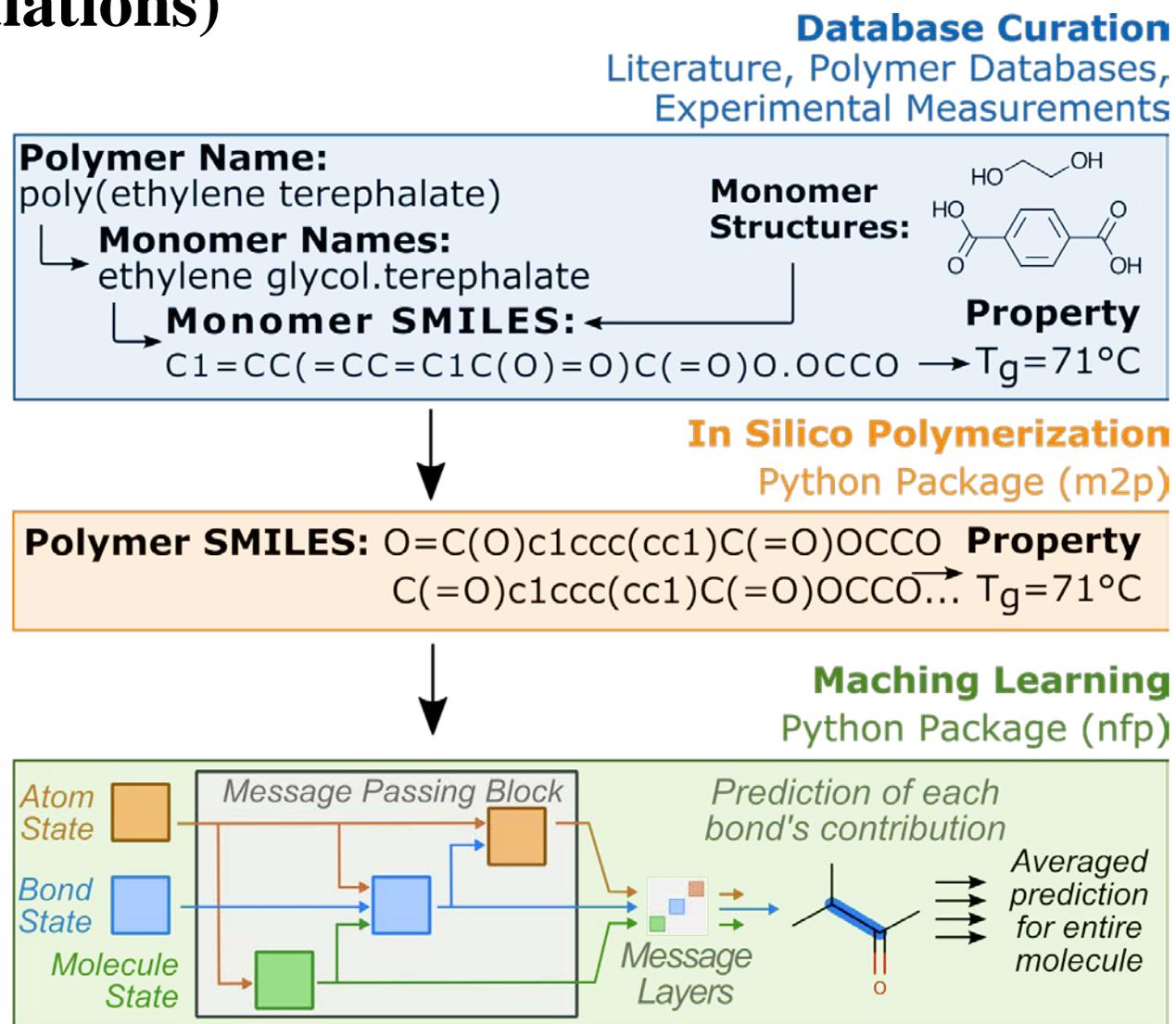
1,2,5,6-hexanetetrol
(tetrol)

→ 300 g of tetrol was synthesized by using a 2L batch reactor

2: Outcomes: We have been using Machine Learning Database (PolyML to screen through Polymer Formulations)

Pipeline Components

- Database - links monomer structure to polymer property (~2,000 unique polymer structures in database)
- Automated, *in silico* structure generation
- Message passing neural network



2: Outcomes: Abbreviations

Monomers = 1,5-pentanediol, adipic acid and furandicarboxylic acid

Polymer = Poly(pentylene adipate-co-furandicarboxylate), **Abberivation** = **PPeC₆F₇₀**

P = Poly

Pe = 1,5-Pentanediol

C₆ = 6 C-atom linear diacid: HOOC(CH₂)₄COOH

F₇₀ = 70 mole% furandicarboxylic acid (FDCA)

Polymer = Poly(pentylene adipate-co-terephthalic acid), **Abberivation** = **PPeC₆T₆₀**

P = Poly

Pe = 1,5-Pentanediol

C₆ = 6 C-atom linear diacid: HOOC(CH₂)₄COOH

T = 60 mole% Terephthalic acid (TPA)

2: Outcomes: FDCA Polymers do not meet the Temperature Specifications

Monomers = 1,5-pentanediol, adipic acid and furandicarboxylic acid

Polymer = Poly(pentylene adipate-co-furandicarboxylate),

Abberivation = **PPeC₆F₇₀**

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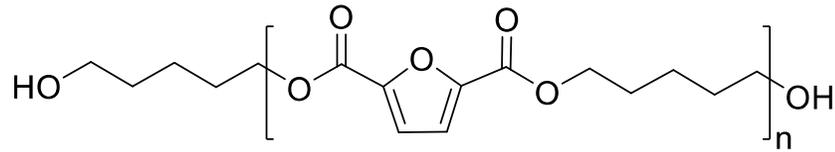
Pe = 1,5-Pentanediol

C₆ = 6 C-atom linear diacid: HOOC(CH₂)₄COOH

T = 60 mole% Terephthalic acid (TPA)

Polymers	T _g (°C)	T _m (°C)	T _m -T _g (°C)
PPeC ₄ F ₅₀	-28.4	-	
PPeC ₆ F ₅₀	-20.9	46.0	66.9
PPeC ₆ F ₇₀	-21.5	44.8	66.3
PPeC ₆ F ₉₀	3.7	55.3	59.0
PPeC ₈ F ₅₀	-39.3	-	
PPeC ₈ F ₇₀	-33.0	44.8	77.8
PPeC ₉ F ₅₀	-37.7	-	
PPeC ₁₀ F ₅₀	-29.2	-	
PPeC ₁₀ F ₇₀	-29.3	46.4	75.7
PPeC ₁₂ F ₅₀	-36.0	34.3	70.3
PPeC ₁₂ F ₆₀	-32.3	40.5	72.8
PPeC ₁₂ F ₇₀	-25.1	38.0	72.8
PPeC ₁₂ F ₈₀	-22.07	41.68	60.2
PPeC ₁₂ F ₉₀	-4.2	56.0	66.3
PPeF ¹	25	95	70.0
PPeF ²	24.8/19.6	76.1/66.2	51.3/46.6
PPeF ³	9.9	66.2	56.7

2: Outcomes: Thermal and Barrier Properties of PPeF by Polycondensation



Poly(pentamethylene furanoate) (PPeF)

PPeF 1

$M_n = 20.9$ kg/mol
 $M_w = 35.7$ kg/mol
 $\bar{D} = 1.7$

$T_d = 341$ °C

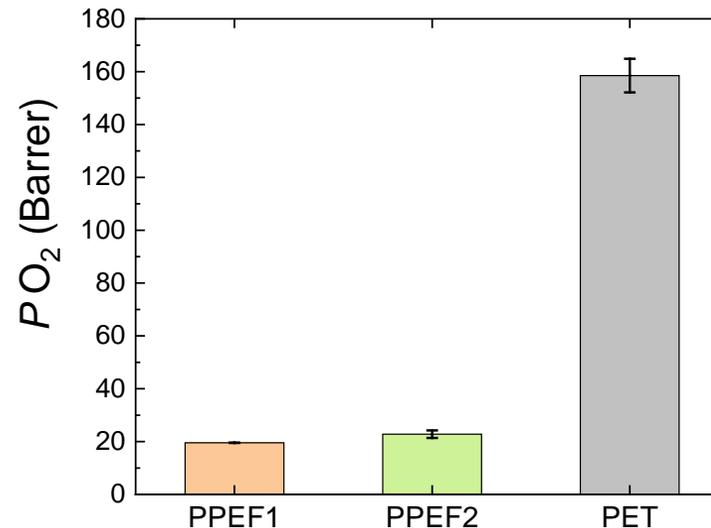
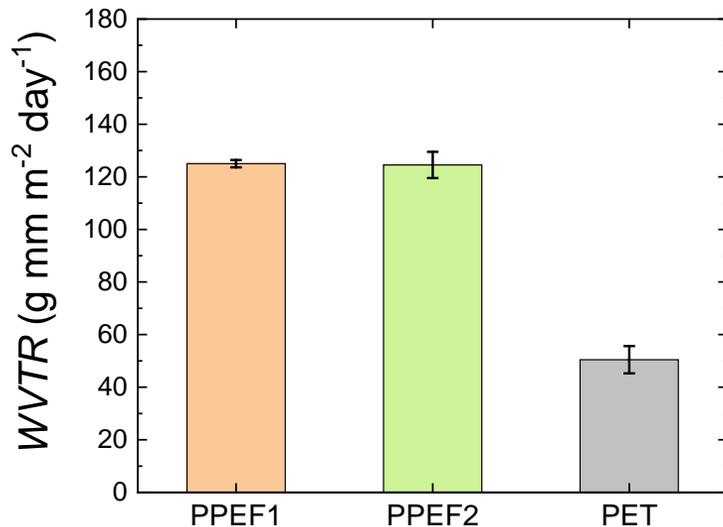
$T_g = 24.8$ °C
 $T_m = 76.1$ °C
 $\Delta H_m = 28.5$ J/g

PPeF 2

$M_n = 26.9$ kg/mol
 $M_w = 37.8$ kg/mol
 $\bar{D} = 1.4$

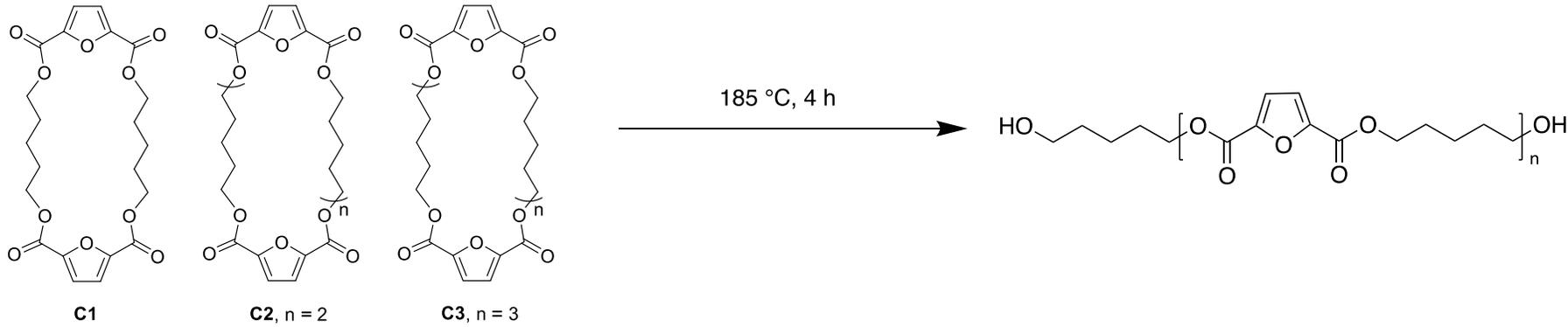
$T_d = 345$ °C

$T_g = 19.6$ °C
 $T_m = 66.2$ °C
 $\Delta H_m = 31.3$ J/g

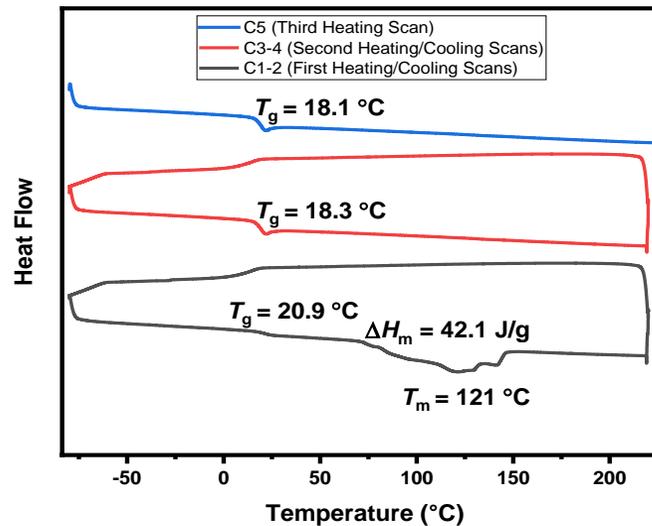
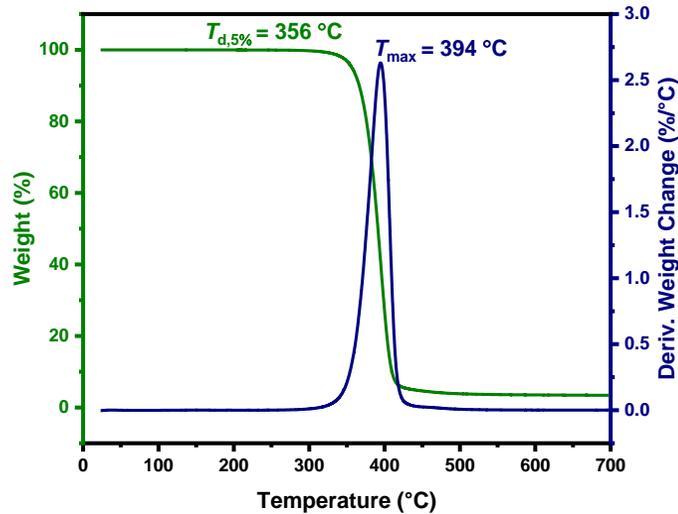


- PPeF showed ~ 8-fold improvement in oxygen barrier over PET
- PPeF, with elongation at break > 1000%, is much more flexible than both PEF and PET

2: Outcomes: Chain-growth ring-opening polymerization route to PPeF



Structurally characterized



- Solvent free, melt polymerization
- High T_m PPeF was achieved
- Depolymerization reforms cyclic macromers C1, C2, and C3
- Potential pathway for chemical circularity



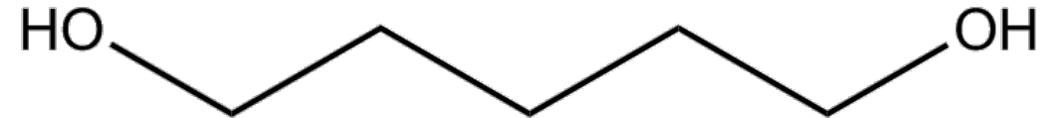
PYRANCO



2:Outcomes

Cost advantaged

- High molar yields (over 85% for entire process)
 - Cheap and stable catalysts
 - Low separation costs

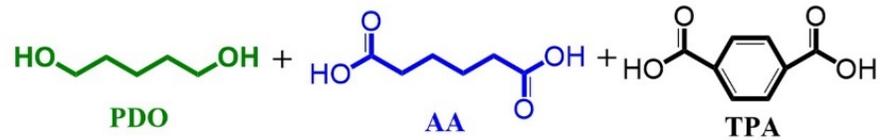


1,5-Pentanediol (1,5-PDO)

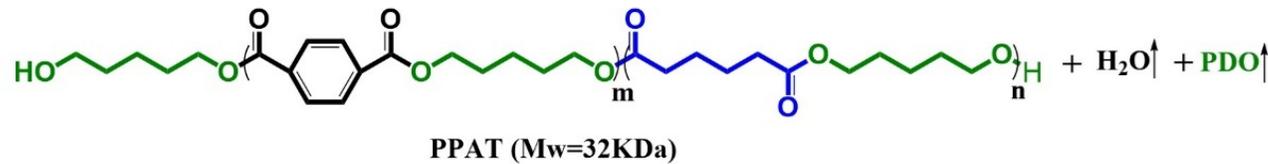
Clean and Renewable

- Clean process – no byproducts, only wastewater treatment
- Renewable biomass-derived feedstock (furfural)
- Over 60% reduction in greenhouse gases (GHGs)

2 Outcomes: Synthesis of PPeC₆T (PPAT)

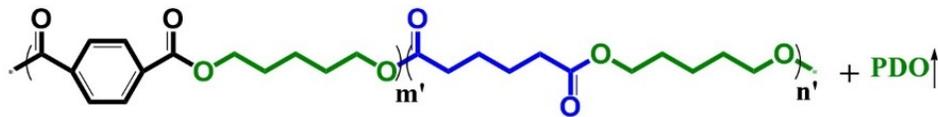


1. Esterification, 175-230°C, 8hrs
2. Polycondensation, 230-250°C, 0.5mbar, 4hrs

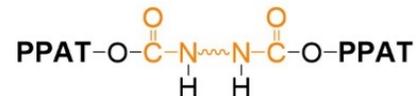


3. Thin-film polymerization

1.6mm melt film
230-250°C, 0.01-0.02mbar, 5-6hrs



3. Chain extension, 200°C, 15mins



Biomass content
PPeC₆T = 42% if only
PDO is from biomass

2 Outcomes: PPeC₆T₆₀ Meets Temperature Specification



PPeC₆T₆₀



PPeC₆T₆₀
0.3 % Glycerol



PPeC₆T₆₀
0.5 % 1,2,5,6-Hexanetetrol

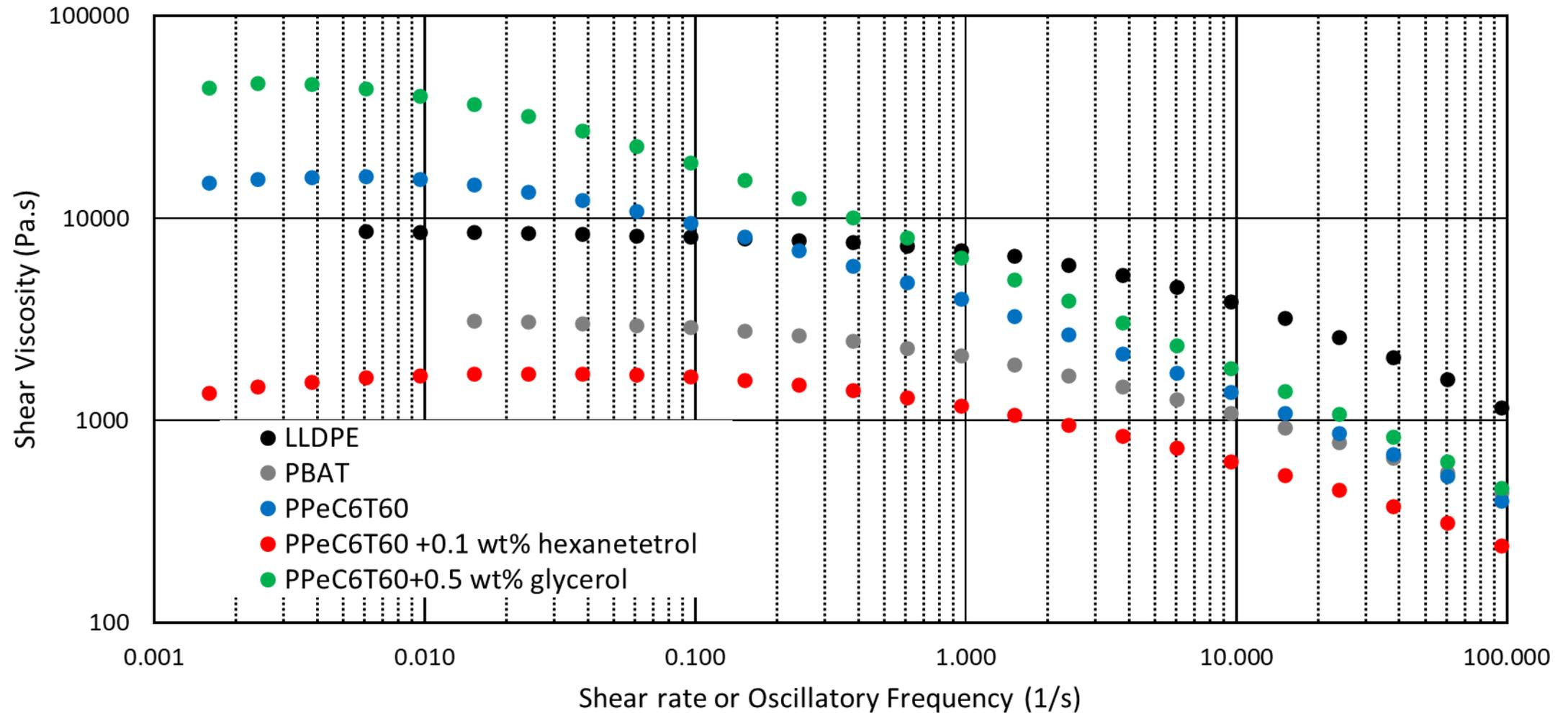
Polymers	T _g (°C)	T _m (°C)	T _m -T _g (°C)	M _n	M _w
PPeC ₆ T ₆₀	-29.1	82.1	114.7	19947	24047
PPeC ₆ T ₇₀	-17.1	96.1	113.2	20710	25375
PPeC ₆ T ₆₀	-9.1	100.8	109.9	106450	188553
PPeC ₆ T ₆₀ + 0.5% Glycerol	-13.3	88.4	101.7	99605	156611
PPeC ₆ T ₆₀ + 0.1% 1,2,5,6-Hexanetetrol	-11.4	99.1	110.5	88433	141278
PBC ₆ T ₅₀ (PBAT)	-30	125	155	97848	148803

May want to reduce slightly T percentage to ~50 to reduce T_g

2 Outcomes: PPeC₆T₅₀ has 75% Higher Modulus of Elasticity Than PBAT

Samples	E (MPa)	δ_y (MPa)	ϵ_y (%)	δ_b (MPa)	ϵ_b (%)
PPeC ₆ T ₆₀	140	11	18	30	801
PPeC ₆ T ₆₀ + 0.5% Glycerol	127	10	14	24	782
PPeC ₆ T ₆₀ + 0.1% 1,2,5,6-Hexanetetrol	140	10	13	17	615
PBAT=PBC ₆ T ₅₀	79	/	/	26	842
LLDPE	201	11	69	31	694

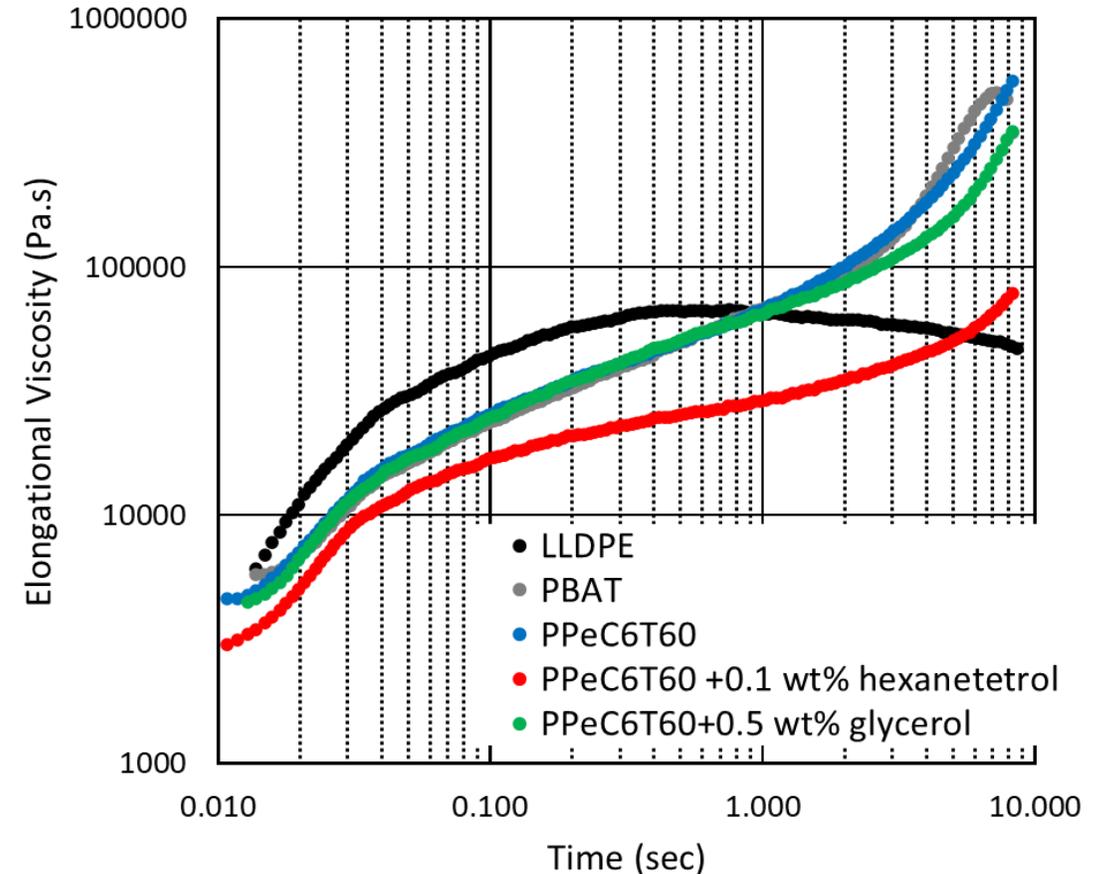
2. Outcomes: Shear Rheology Comparison at 190°C



2 Outcomes: Extensional Viscosity at 130°C and 0.3 s⁻¹

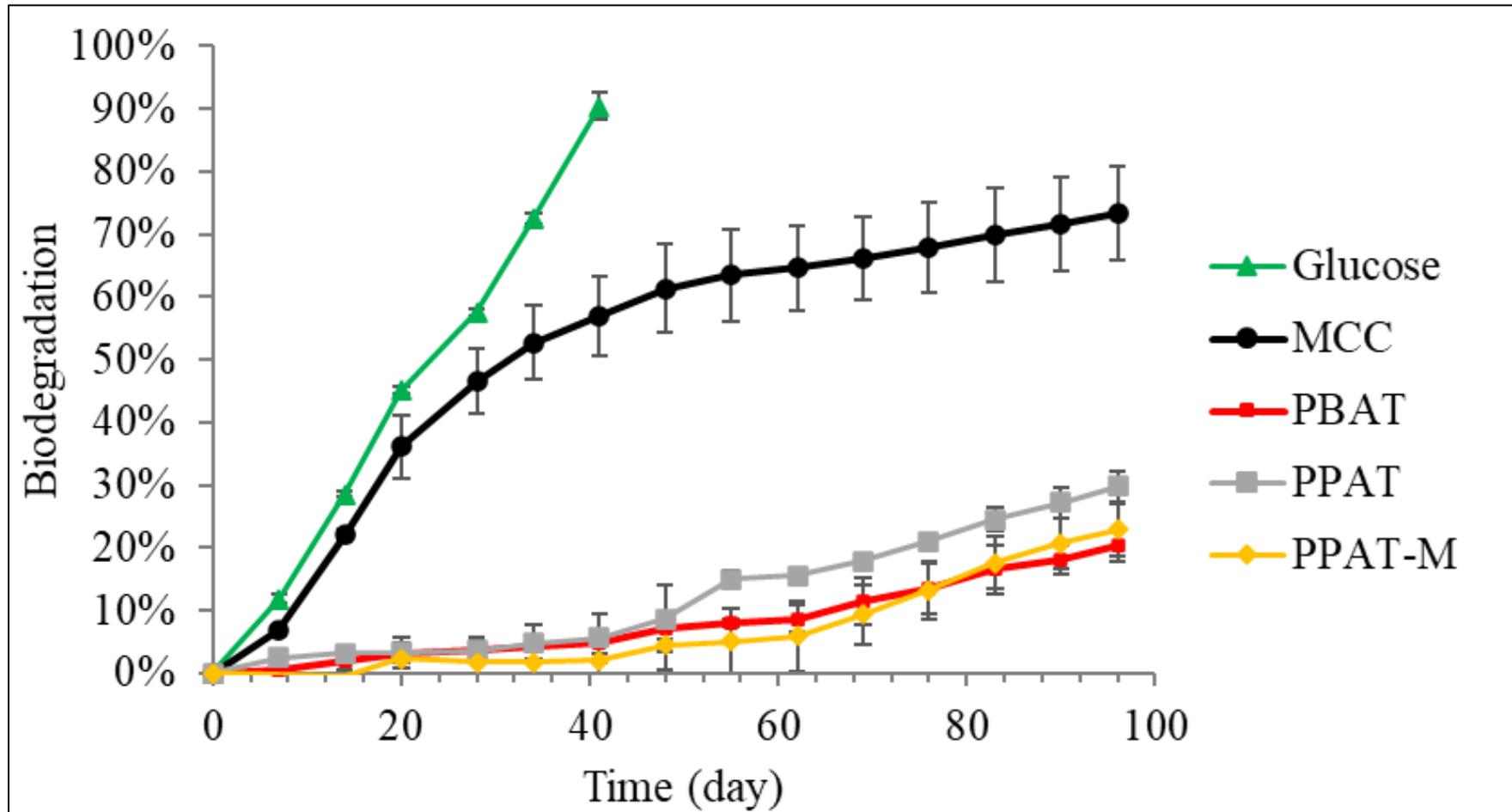
(Value at Hencky strain of 2.5)*

Samples	η_E (Pa*s)
PPeC ₆ T ₆₀	562294
PPeC ₆ T ₆₀ + 0.5% Glycerol	350234
PPeC ₆ T ₆₀ + 0.1% 1,2,5,6-Hexanetetrol	78102
PBAT=PBC ₆ T ₅₀	349278
LLDPE	46833



*A Hencky strain of 2.5 at an elongational rate of 0.3 s⁻¹ were found to be representative values for the film blowing (Härth and Dörnhöfer, Polymers 2020, 12, 1605)

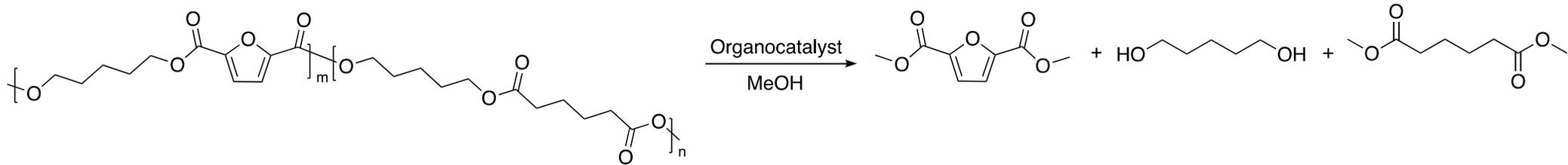
2 Outcomes: PPeC₆T or PPAT has similar soil and aquatic biodegradability as PBAT



Lei Zheng, Min Soo Kim, Shu Xu, Meltem Demirtas, George W Huber, John Klier, Biodegradable high molecular weight poly (pentylene adipate-co-terephthalate): synthesis, thermo-mechanical properties, microstructures, and biodegradation (submitted)

2 Outcomes: Methanolysis as a recycling strategy

Sample depolymerization reaction:

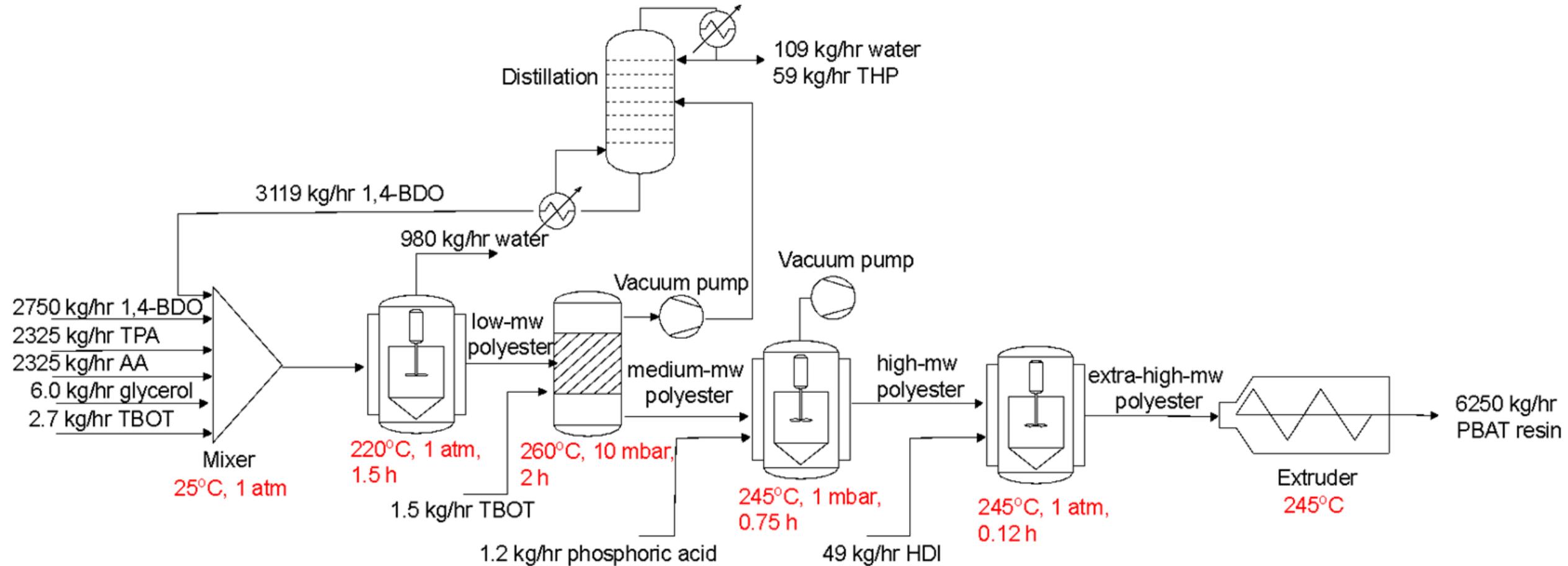


Analytical Strategy: Quantify monomer products by a combination of HPLC-UV and HPLC-MS with instruments that already exist at NREL

Reaction progress can also be assessed by NMR spectroscopy and GPC analysis of reaction samples

2 Outcomes: Process Flow Diagram for PBAT

(Basis: 50,000 tons/year)



The overall goal of this project is to design **new biomass-based polyesters** that have improved thermal or mechanical properties compared to PBAT and are also chemically recyclable and biodegradable. We will test these polyesters in three different commercial applications.

The goal of this project is to design a new class of polyesters with the following properties:

1. **50 to 70%** lower energy input than conventional petroleum polymers. (currently >26% lower if PDO from biomass more if TPA and AA come from biomass)
2. Biomass based content from **50 to 100 wt%**. (Currently 22% with PDO from biomass and other monomers from petroleum more if TPA and AA come from biomass)
3. Costs **30-50%** lower than PBAT. (Currently >25% lower depending on scale)
4. **60%** biodegradable in 180 days by ASTM D6400.
5. Modulus at least **200 MPa** and elongation at break at least 350% (similar to LDPE and linear-low density poly-ethylene (LLDPE)). (140% improvement compared to PBAT)
6. Melting temperature **105-115°C** (similar to LDPE and LLDPE). (95-105 C)
7. Haze index for a 25 μm film ~ 10 according to ASTM D1003 (similar to LDPE and LLDPE). (working on testing)
8. O₂ transmission rate equal to or lower than $\sim 8000 \text{ cm}^3/(\text{m}^2 \text{ day})$ (LDPE and LLDPE).

3 – Impact

- Creating new biomass-based biodegradable polymers
- Have improved economics and environmental impacts compared to existing biodegradable PBAT/PLA blends
- Provide new markets for biomass- monomers
- Finding new applications for bio-based polymers (improved barriers, biodegradability)

Additional Slides

Responses to Previous Reviewers' Comments

- No previous comments

Publications, Patents, Presentations, Awards, and Commercialization

- Lei Zheng, Min Soo Kim, Shu Xu, Meltem Demirtas, George W Huber, John Klier, Biodegradable high molecular weight poly (pentylene adipate-co-terephthalate): synthesis, thermo-mechanical properties, microstructures, and biodegradation (submitted)
- MS Kim, Hochan Chang, Lei Zheng, Qiang Yan, Brian F Pflieger, John Klier, Kevin Nelson, Eric L. –W Majumder, George W. Huber, A Review of Biodegradable Plastics: Chemistry, Applications, Properties and Future Research Needs, (submitted)
- Raka G Dastidar, Min Soo Kim, Panzheng Zhou, Zaneta Luo, Changxia Shi, Kevin J Barnett, Daniel J McClelland, Eugene Y-X Chen, Reid C Van Lehn, George W Huber, [Catalytic production of tetrahydropyran \(THP\): a biomass-derived, economically competitive solvent with demonstrated use in plastic dissolution](#), Green Chemistry, (2022) 24,23, 9101-9113.

Task	Year 1				Year 2				Year 3			
	Q1	Q2	Q3	Q4	Q5	Q6	Q7	Q8	Q9	Q10	Q11	Q12
Task 1: Initial Verification	←											
M1.1-1.3: Verification of synthesis, biomass-monomers and PolyML	●—●											
M1.4: DOE verification of experimental data process models from proposal(Go/No-Go/SMART)	★											
Task 2: Synthesis/characterization of polyesters	←											
M2.1.1: Properties 1,5-PDO polyesters with PolyML	●—●											
M2.1.2, M2.1.3: Synthesis of 1,5-PDO polyesters (SMART)	●—●											
M2.1.4 - M2.1.8: Properties of 1,5-PDO polyesters	●—●											
M2.2.1: Properties of THFDM, HAH, FDM polyesters with PolyML	●—●											
M2.2.2, M2.2.3: Synthesis of THFDM/FDM + TPA + AA and THFDM/FDM + FDCA	●—●											
M2.2.4-M2.2.8: Properties THFDM/FDM polyesters	●—●											
M2.3: Improve accuracy of PolyML.	●—●											
M2.4: Identify the least expensive biomass-based polyester compared to PBAT and optimal properties for film applications (Go/No-Go/SMART)								★				
Task 3: Chemical Recycling of Polyesters	←											
M3.1.1, M3.1.2: Recycling of up to 80% of 1,5-PDO polyesters back into monomer components (SMART)	●—●											
M3.2.1, M3.2.2: Recycling of up to 80% of THFDM, FDM polyesters back into monomer components	●—●											
Task 4: TEA and LCA	←											
M4.1-4.2: TEA and LCA model for production and recycling of 1,5-PDO derived polyesters	●—●											
M4.3- M4.4: TEA and LCA model for THFDM/FDM derived polyesters and recycling	●—●											
Task 5: Scaling of Polyester and Application	←											
M5.1, M5.2: Scaling polyester to 2.5 kg/week									●—●			
M5.3-M5.5: Testing of biomass-derived polyester in 3 applications									●—●			
M5.6, M5.7: Refined TEA and LCA.									●—●			
End of Project Goals: M 5.1-M5.7 Write publication, patents, DOE final report. (SMART)									●—●			

★ Go/No-Go ●—● Ongoing Work ← Task Duration